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Claims

1. A process for polymerizing one or more alpha-olefins comprising the following steps:

- a) contacting in a continuous way one or more of said alpha-olefins with a metallocene-based catalyst system in a loop reactor, wherein:
 - (i) the reaction is carried out in a liquid medium;
 - (ii) the average residence time of the metallocene-based catalyst system is not more than 30 minutes;
 - (iii) the temperature ranges from 25° to 70°C;

in order to obtain a polymerization degree ranging from 60 to 500 g per gram of catalyst system;

- b) feeding in continuous the prepolymerized metallocene-based catalyst system obtained in step a) into a polymerization reactor;
- c) polymerizing one or more alpha-olefins, the same or different from the alphaolefins used in step a), in the presence of said prepolymerized metallocenebased catalyst system.
- 2. The process according to claim 1 wherein the prepolymerization step a) is carried out in the presence of hydrogen.
- 3. The process according to claim 2 wherein the prepolymerization step a) the amount of hydrogen present in the loop reactor preferably ranges from 5 to 1000 ppm.
- 4. The process according to anyone of claims 1-3 wherein the average residence time in step a) is not more than 20 minutes.
- 5. The process according to anyone of claims 1-4 wherein in step a) the polymerization degree of the prepolymerized metallocene-based catalyst system ranges from 70 to 300 g per gram of catalyst system.
- 6. The process according to anyone of claims 1-5 wherein in step a) the temperature ranges from 30°C to 65°C;
- 7. The process according to anyone of claims 1-6 wherein the metallocene-based catalyst system is obtainable by contacting:
 - a) at least a transition metal compound containing at least one π bond;
 - b) at least an alumoxane or a compound able to form an alkylmetallocene cation; and
 - c) optionally an organo aluminum compound.

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8. The process according to claim 7 wherein the metallocene-based catalyst system is supported on an inert carrier.

- 9. The process according to anyone of claims 1 to 8 wherein step a) of the process is carried out in the loop reactor (1), then the catalyst-prepolymer product is transferred to separator (2) via line (C), and then via line D to the gas-phase reactor (3) and the polymer is withdrawn through line (F).
- 10. The process according to anyone of claims 1 to 8 wherein step a) of the process is carried out in the loop reactor (1), then the catalyst-prepolymer product is transferred via line (C), to the gas-phase reactor (2) and the polymer is withdrawn through line (D).
- 11. The process according to anyone of claims 1 to 8 wherein step a) of the process is carried out in the loop reactor (1), the catalyst-prepolymer product is transferred to the loop polymerization reactor (2) via line (C) and the polymer is withdrawn through line (E).
- 12. The process according to anyone of claims 1 to 8 wherein step c) is carried out in one or more reactor connected in series.
- 13. The process according to anyone of claims 1 to 12 wherein one or more alpha-olefins of formula CH₂=CHT wherein T is a hydrogen atom or a C₁-C₂₀ alkyl radical and optionally polyenes are homopolymerized or copolymerized.
- 14. The process according to claim 13 wherein propylene is homopolymerized.
- 15. The process according to claim 13 wherein propylene is copolymerized with ethylene or with one or mere alpha olefins of formula CH₂=CHT¹ wherein T¹ is a C₂-C₂₀ alkyl radical and optionally with polyenes.
- 16. The process according to claim 15 wherein propylene and ethylene are copolymerized.